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Abstract: The effects of nonlinear ultrasonic propagation on high-speed ultrasonic gas flow measurement are analyzed based on the sound line equation derived from Snell’s geometric acoustic law. A mathematical model for the ultrasonic propagation path in ultrasonic flowmeter pipe is built, and the relationship between $x$ and $r$ is calculated by MATLAB programming and ode45 simulating. The ultrasonic propagation path at the flow rate of 3~30m/s is simulated in the assumed boundary conditions of the pipeline, transducer installation and fluid state. It shows that the nonlinear propagation characteristics cause the large deviations of the position of received ultrasonic waves in conditions of different flow rates, which strongly affects the stability and accuracy of flow measurement. The simulated offset data of the receiving position are useful for the high-speed gas ultrasonic flowmeter installation and dry calibration on clamp-on ultrasonic flowmeters.

Keywords: Numerical Simulating, Ultrasonic Propagation, Ultrasonic Gas

1. Introduction

As a non-intrusive flow measurement device, the ultrasonic flowmeter has a unique advantage in flammable and explosive gas flow measurement. In the large-diameter pipe natural gas transmission industry, the pipeline flow rate in medium-pressure gas transmission is mostly restricted to 10 m/s or so. In order to improve gas transport efficiency, the natural gas transmission speed is increased to 15m/s ~ 20m/s under 0.2MPa ~ 0.4MPa, the steam transmission speed is mostly controlled in the range of 30m/s ~ 40m/s, and the superheated steam flow rate is more than 60m/s. Hydrogenation in the hydrogen stations generally uses small diameter pipe(15mm ~ 18mm) at the pressure of 30MPa or more, and the hydrogen flow rate is more than 65m/s. Recently, the hydrogenation pressure is increased to 70MPa or 75MPa, and the calculated hydrogen flow rate is 120m/s or more. However, due to the effects of the flow rate on nonlinear ultrasonic propagation, most of the ultrasonic gas flowmeters’ measurement range is less than 30m/s. This paper mainly considers the application of the ultrasonic flowmeter for high-speed gas flow measurement. At first, the ultrasonic propagation characteristics in the high-speed gas medium are analyzed, then, the effects of the flow rate on nonlinear ultrasonic propagation are simulated to provide the theoretical and methodological bases to develop the high-speed gas ultrasonic flowmeter.

Some researchers have studied the nonlinear characteristics of ultrasonic propagation. Vanhille et al. [1] simulated the nonlinear ultrasound propagation properties in the fluid with the Lagrangian equation, and they mainly studied the nonlinear relationship between the sound pressure and the propagation distance. Willatzen et al. [2, 3] studied the non-linear relationship between the propagation time and the flow rate based on the fluid dynamic equations and the basic formula for measuring the flow rate. Q. Ji et al. [4–9] studied the ultrasonic propagation characteristics and model in aluminum, colloids and other materials. Francesco Lanza di Scalea et al. [10] observed and measured the ultrasonic propagation characteristics through establishing the physical experimental apparatus and mainly studied the relationship between the re-
have established successively the relevant standards of gas and natural gas flow measurement for ultrasonic flowmeters, in which the ultrasound propagates in the pipeline from the emitting transducer to the receiving by the S-shaped path, and the ultrasonic propagation equation determined by Snell’s law is presented roughly. However, a few papers have been reported about the relationship between the nonlinear ultrasonic propagation path and the flow rate. So, this work mainly deals with the effects of flow rates on ultrasonic propagation path based on the ultrasonic propagation equation determined by Snell’s law and the wave propagation trajectory equation derived by Boone and Vermaas.

2. Ultrasonic propagation model in the ultrasonic flowmeter pipe

The structure of the typical clamp-on ultrasonic flowmeter investigated in this work is shown in Fig.1 [13], and it consists of clamp holder, upstream and downstream transducers, preamplifier, and ultrasonic flowmeter. It is the typical structure of the small diameter clamp-on ultrasonic flowmeters in American GE, German Flexim, Japan’s Fuji Corp etc. According to GB/T18604-2001 and AGA Report No.9, the average axial flow velocity formula for transit-time single path ultrasonic flowmeter is:

\[
V = K_C \frac{L}{2 \cos \phi_0} \cdot \frac{t_U - t_D}{t_D t_U},
\]

(1)

The related parameters are shown in Fig.2, where, \(L\) is the straight line length between the ultrasonic sensors \(A\) and \(B\), and \(\phi_0\) is the initial transmission angle for the ultrasonic path. In equation (1), \(t_D\) is the ultrasonic downstream propagation time, \(t_U\) is the ultrasonic upstream propagation time, and \(K_C\) is the velocity distribution coefficient.

As the flow rate along the pipe cross-section is not constant, the ultrasonic wave propagation path in the pipeline is not linear. According to velocity distribution function \(V(r)\) and Snell’s geometrical acoustic law, the ultrasonic transmission line equation is determined as

\[
\frac{C}{\cos \phi(r)} + V(r) = \text{Const},
\]

(2)

Where, \(C\) is the ultrasonic propagation velocity in air.

According to Boone and Vergas’s model, the acoustic line equation is written as:

\[
\begin{align*}
\frac{dx}{dt} &= C \times \cos \phi(r) + V(r) \\
\frac{dr}{dt} &= C \times \sin \phi(r) \\
\frac{d\phi}{dr} &= -\cos^2 \phi(r) \frac{dV(r)}{dr}
\end{align*}
\]

(3)

Where, \(x\) is the ultrasonic propagation horizontal displacement from the transmitting sensor as a starting point, \(r\) is the ultrasonic propagation radial displacement, and \(\phi(r)\) is the angle between the particle motion tangent and the axis in position \(r\) of ultrasonic propagation path.

According to the empirical formula of Prandtl velocity distribution, and considering the fully developed turbulent flow, the velocity distribution is:

\[
V(r) = V_m(1 - \frac{|r|}{R})^{\frac{n}{2}},
\]

(4)

Where, \(V_m\) is the surface velocity along the axial line, and \(R\) is the radius of the pipeline. Considering only the smooth pipe, the index \(n\) is:

\[
n = 2 \log_{10}\left(\frac{R}{D}\right) - 0.8,
\]

(5)

Where, \(Re\) is Reynolds number of fluid in the pipeline which is defined as \(Re = \frac{V D}{\nu}\), and \(\nu\) is the viscosity coefficient.

The mean flow velocity \(V_z\) on the vertical center parallel pipeline section and the pipeline mean flow velocity \(V\) both are defined respectively as

\[
V_z = \frac{1}{L} \int V(r) dL,
\]

(6)

\[
V = \frac{1}{S} \int S V(r) dS,
\]

(7)

Where, \(L\) is the ultrasonic path length; \(S\) is the pipeline inner sectional area. So the relation of \(V_z\) and \(V\) is:

\[
V = \frac{2n}{(2n + 1)} V_z.
\]

(8)

Eq.(8) is compared with Eq.(1), and there are definitions as follows

\[
K_C = \frac{2n}{(2n + 1)},
\]

(9)

\[
V_z = \frac{L}{2 \cos \phi_0} \cdot \frac{t_U - t_D}{t_D t_U},
\]

(10)

From Eq.(3) and Eq.(4), according to the downstream and upstream situations a model is established as follows:

(1) Ultrasonic propagation in the downstream direction

The relationship of \(\phi\) and \(r\) can be derived as:

\[
\begin{align*}
\frac{d}{dr} &= \frac{-nRc \sin \phi}{v_m \cos^2 \phi (1 - \frac{r}{R})^{n-1}} \quad 0 \leq r \leq R \\
\frac{d}{dr} &= \frac{-nRc \sin \phi}{v_m \cos^2 \phi (1 + \frac{r}{R})^{n-1}} \quad -R \leq r \leq 0
\end{align*}
\]

(11)

And the relationship of \(x\) and \(r\) is obtained as:

\[
\begin{align*}
\frac{d}{dr} &= \frac{-c \sin \phi}{v_m (1 - \frac{r}{R})^2 + c \cos \phi} \quad 0 \leq r \leq R \\
\frac{d}{dr} &= \frac{c \sin \phi}{v_m (1 + \frac{r}{R})^2 + c \cos \phi} \quad -R \leq r \leq 0
\end{align*}
\]

(12)
3. Simulation and analysis of models

3.1. Method

According to Eq. (11) and Eq. (13), the results can be derived as follows:

(1) Ultrasonic propagation in the downstream direction:

\[
\begin{align*}
\cos \phi &= \frac{c}{c \cos \varphi_0 - R_v (1 - \frac{c}{R})}, \quad 0 \leq r \leq R \\
\cos \phi &= \frac{c}{c \sec \varphi_0 - R_v (1 + \frac{c}{R})}, \quad -R \leq r \leq 0
\end{align*}
\]  

(15)

(2) Ultrasonic propagation in the upstream direction:

\[
\begin{align*}
\cos \phi &= \frac{c}{c \sec \varphi_0 + R_v (1 - \frac{c}{R})}, \quad 0 \leq r \leq R \\
\cos \phi &= \frac{c}{c \sec \varphi_0 + R_v (1 + \frac{c}{R})}, \quad -R \leq r \leq 0
\end{align*}
\]  

(16)

When Eq. (15) is put into (12), and (16) into (14), a complex equation can be derived, and it is difficult to solve the integral directly. With the numerical solution method of ordinary differential equation MATLAB ode45, the relationship of \( \phi \) and \( r \) can be solved. Using the Runge-Kutta algorithm, ode45 is a variable step size solver. Ode45 has fourth-order and fifth-order Runge-Kutta single-step algorithm. Its truncation error is \( (\Delta x) 3 \). It can be mainly used to solve Nonstiff (non-rigid) of ordinary differential equations, and it is the preferred method to solve the problem of numerical solution.

3.2. Discussion

The measurement pipeline condition is assumed as \( R = 100 \text{mm} \) and \( c = 340 \text{m/s} \), and the initial ultrasound launch angle is \( \phi_0 = 30^\circ \).

If \( Re = 4e6, n = 10.3724 \).

The ultrasonic propagation trajectory under

\[ V = \{12, 15, 18, 24, 27, 30\} \text{(m/s)} \]

is calculated and depicted by calculating and simulating with MATLAB and ode45.

Fig.3 and Fig.4 show respectively ultrasound downstream and upstream transmission paths at higher flow rates. In order to show the level migration of ultrasonic wave reaching the end of the pipeline wall at the different flow rates more clearly. Fig. 3 and 4 are respectively enlarged partly as shown in Fig. 5 and 6.

In Fig.3 ~ Fig.6, the solid line is the ultrasonic propagation path at zero fluid velocity. The others are the ultrasonic propagation paths from the left to the right at \( V = \{12, 15, 18, 24, 27, 30\} \text{(m/s)} \). As can be seen from Fig. 3 and Fig. 5, the deviation from the zero velocity of ultrasonic downstream propagation paths is larger with the higher flow rate. As shown in Fig. 4 and Fig. 6, the deviation from the zero velocity of ultrasonic upstream propagation paths is larger too with the higher flow rate. However, as presented in Fig. 5 and Fig. 6, the downstream offset is larger clearly than the upstream one, and is about 2 times that of the upstream.

In order to compare the offsets of ultrasonic propagation path to reach the end of the pipeline wall under the lower flow rates, Fig. 7 and Fig. 8 show propagation paths of the ultrasonic wave respectively calculated by MATLAB and ode45 at \( V = 3 \sim 12 \text{m/s} \) in downstream and upstream. Fig. 3 ~ 8 shows that the maximum offsets of the pipeline end of ultrasonic propagation path under the high speed fluid are 2 times or more than under the zero speed fluid. Through calculating by MATLAB programming, when \( V = 30 \text{m/s} \), the displacement of ultrasonic downstream propagation in x direction is obtained, i.e. \( X_{30} = 0.363 \text{m} \). When \( V = 0 \text{m/s} \), the displacement is obtained, i.e. \( X_0 = 0.346 \text{m} \) and then the offset of ultrasonic downstream propagation is \( \Delta x = X_{30} - X_0 = 0.015 \text{m} \). The same method can be used to calculate the offset of ultrasonic upstream propagation, that is, \( \Delta xU = 0.007 \text{m} \). By this way, the above conclusion is verified.
Figure 2 ultrasonic propagation in the pipeline.

Figure 3 ultrasonic downstream propagation path in High-velocity fluids.

Figure 4 ultrasonic upstream propagation path in High-velocity fluids.

Figure 5 the enlargement diagram of ultrasonic downstream propagation path in High-velocity fluids.

Figure 6 the enlargement diagram of ultrasonic upstream propagation path in High-velocity fluids.

Figure 7 the enlargement diagram of ultrasonic downstream propagation path in Low-velocity fluids.
4. Conclusion

Theoretically, with analysis on nonlinear character of the ultrasonic propagation in gas flow measurement, we have drawn the conclusion that the nonlinear ultrasonic propagation causes a deviation of ultrasonic wave reaching the end of the pipeline wall from the receiving ultrasonic sensor. Since the position of received ultrasonic wave changes at the flow rate, the position will deviate from the center of the receiving ultrasonic sensors’ effective area (usually with the diameter of 7 ∼ 12mm), especially at the higher flow rate. The propagation time also changes with the flow rate, which affects the accuracy of the ultrasonic flowmeter. According to the above simulation results, the maximum offset is 15mm at the flow rate V=30m/s, and will be even greater for the higher speed fluid. So, the large-diameter insert-type ultrasonic gas flowmeter can be usually used at the occasions of the relatively steady flow field and flow velocity. And for the clamp-on ultrasonic gas flowmeter, two movable ultrasonic sensors can be designed to improve the flow measurement stability and accuracy. The above simulating results are very useful for the high-speed ultrasonic gas flowmeter installation and the dry calibration on clamp-on ultrasonic flowmeters.

References


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